

# MYRRHA Primary Heat Exchanger stability analysis

Diego Castelliti  
SCK•CEN  
diego.castelliti@sckcen.be



IRUG 2014 Meeting  
11-12 September 2014  
INL – Idaho Falls

- MYRRHA plant: purposes and general design
- MYRRHA Primary Heat eXchanger (PHX) general description
- MYRRHA preliminary control strategy
- Two-phase system-dependent instabilities types
  - Ledinegg instability
  - Density Wave Oscillation (DWO) instability
  - Flow regime-induced instability
- Orifice dimension
- Induced stability criterion

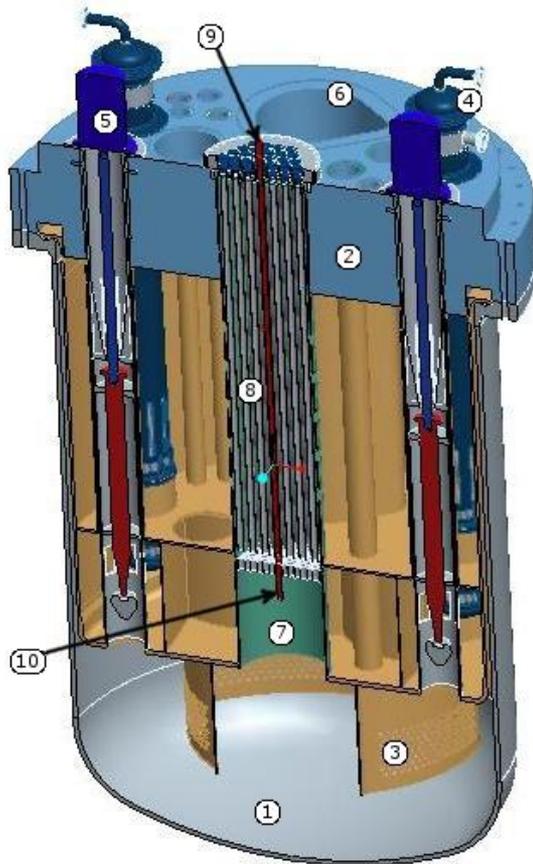
# MYRRHA plant: purposes and general design

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- MYRRHA: Multi-purpose hYbrid Research Reactor for High-tech Applications
- Pool-type Accelerator Driven System (ADS) with ability to operate also as critical reactor
- Liquid Lead-Bismuth Eutectic (LBE) as primary coolant
- Main purposes:
  - Flexible irradiation facility
  - Minor Actinides (MAs) transmutation demonstration in support of R&D on a "closed fuel cycle" (Generation IV requirement)
  - ADS demonstrator
  - Lead Fast Reactor demonstrator
  - (Pre-) Gen IV plant
- MYRRHA project recognized as high priority infrastructure for nuclear research in Europe

# MYRRHA plant: purposes and general design

- MYRRHA primary system design current status (design revision 1.6):



1. Reactor vessel
2. Reactor cover
3. Diaphragm
4. Primary heat exchanger
5. Pump
6. In-Vessel Fuel Handling Machine
7. Core barrel
8. Above Core Structure
9. Core plug
10. Spallation window

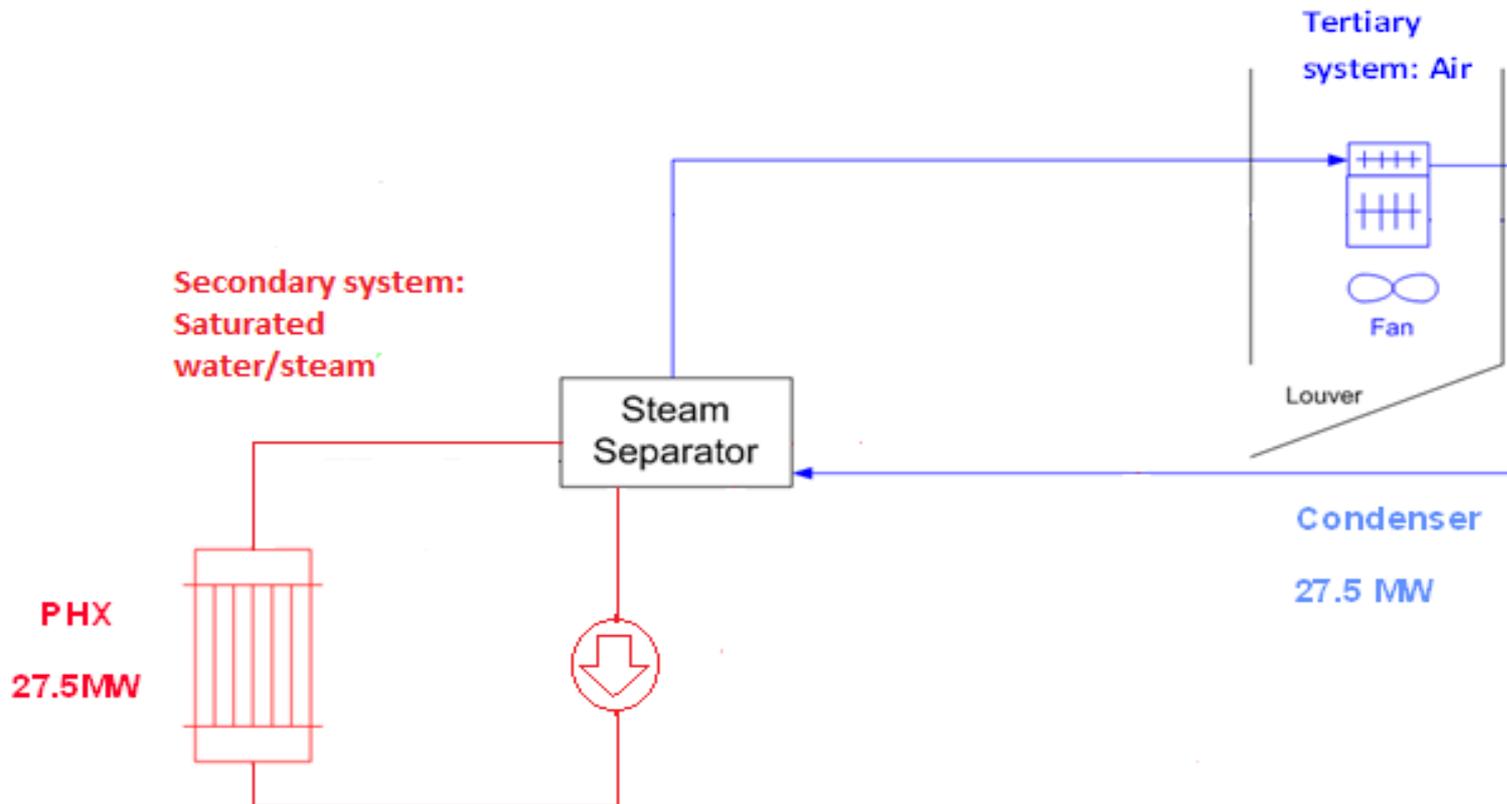
# MYRRHA plant: purposes and general design

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- Primary system:
  - Completely enclosed in primary vessel (pool-type)
  - Primary LBE flow path:
    - Lower plenum (270 °C)
    - Core (100 MW)
    - Upper plenum (~325 °C)
    - 4 Primary Heat eXchanger (PHX) units
    - 2 Primary Pumps (PPs)
    - Lower plenum
  - Cold plenum separated from hot plenum by Diaphragm supporting core barrel and components' penetrations
  - Above LBE free surface: Nitrogen layer

# MYRRHA plant: purposes and general design

- MYRRHA secondary system (one loop out of four) design state of the art (developed in FP7 Central Design Team project):



# MYRRHA plant: purposes and general design

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- Secondary system:
  - Four independent secondary loops (linked through PHXs)
  - Operated with forced flow two-phase water mixture (16 bar, 200 °C)
  - Secondary water flow path:
    - PHX inlet ( $\sim$ saturated conditions)
    - PHX outlet ( $x \sim 0.3$ ,  $\alpha \sim 0.9$ )
    - Moisture separated in steam drum
  - In normal operation, secondary water temperature kept constant by control system (primary LBE temperature changing as a function of core loading)
- Tertiary system: dissipating heat to external environment through air condensers (forced circulation air fans)
- Condensed steam recirculated into steam drum

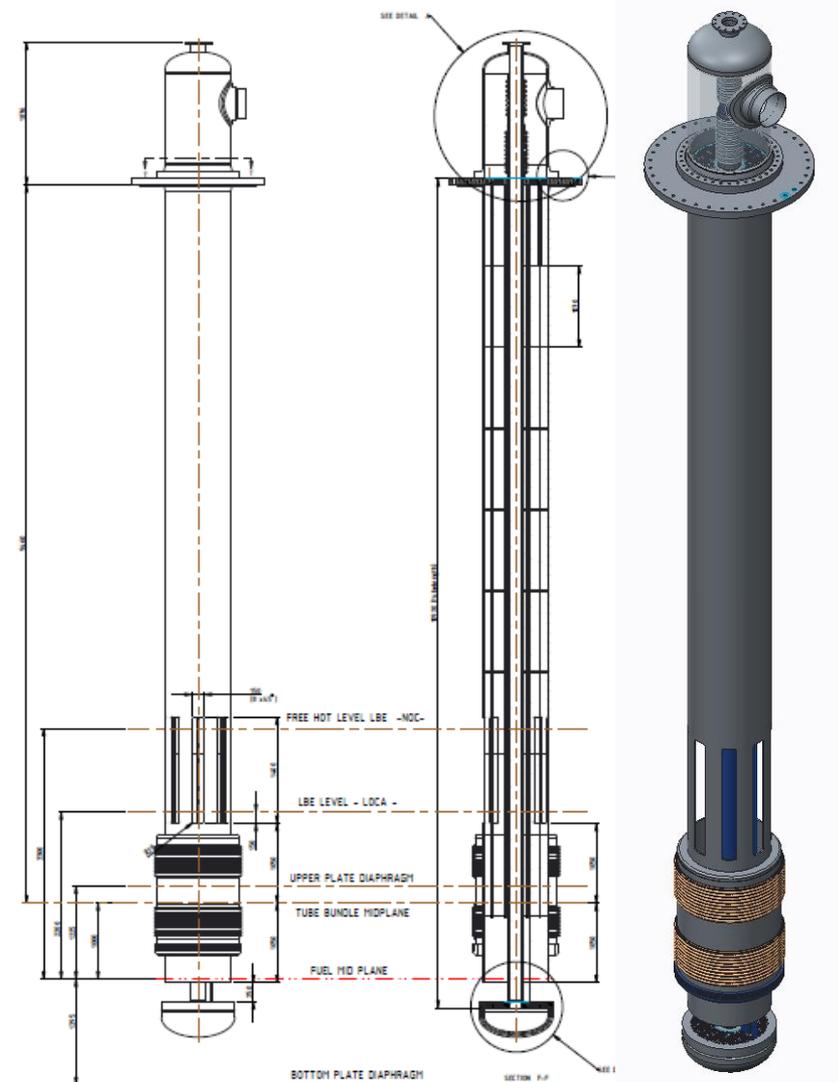
# MYRRHA plant: purposes and general design

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- MYRRHA plant designed for 110 MW as nominal power:
  - 100 MW → core power
  - 10 MW → additional heat sources:
    - In Vessel Storage Tank (IVST)
    - Po decay heat
    - Pump power
    - $\gamma$  heating
    - Spallation target power
- Normal operation → all three cooling systems designed to operate in forced circulation
- Accidental conditions → DHR in full natural circulation (three cooling loops operating in passive mode)
- Two systems to remove decay heat power:
  - DHR-1: secondary and tertiary systems operating in passive mode
  - DHR-2: Reactor Vessel Auxiliary Cooling System (RVACS)

# MYRRHA PHX general description

- MYRRHA PHX: counter-current shell-and-tube concept:
  - 684 stainless steel (AISI 316L) tubes
  - Wall thickness = 1 mm
  - 2 tube plates (thickness = 80 mm)
  - Double-walled central feedwater pipe
  - Double-walled bottom head
  - Top head
  - External shroud



# MYRRHA PHX general description

- MYRRHA PHX main geometrical and thermal-hydraulical parameters:

Parameter	Unit	Value
Power in one PHX	MW	27.5
Shroud external diameter	mm	850
Shroud internal diameter	mm	820
Feed water pipe external diameter	mm	200
Water tubes number	-	684
Water tubes pitch	mm	26
Water tubes external diameter	mm	16
Water tubes internal diameter	mm	14
Thickness of water tubes	mm	1
<b>Total length of water tubes</b>	mm	10920
<b>Active length of water tubes</b>	mm	2100

MYRRHA PHX main geometrical parameters

Parameter	Unit	Value
PHX LBE inlet temperature	°C	325
PHX LBE outlet temperature	°C	270
LBE safe shutdown temperature	°C	200
PHX LBE mass flow rate	kg/s	3450
<b>PHX water inlet temperature</b>	°C	200
<b>PHX water outlet temperature</b>	°C	201.4
PHX water mass flow rate	kg/s	47
<b>PHX water pressure</b>	bar	16
<b>PHX water outlet quality</b>	-	0.3
<b>PHX water outlet void fraction</b>	-	0.9
LBE velocity	m/s	0.93
Primary side LBE pressure drop	bar	0.04
Water outlet velocity	m/s	3.3
Steam outlet velocity	m/s	18.63
Secondary side water pressure drop	bar	0.95

MYRRHA PHX main thermal-hydraulical parameters

# MYRRHA PHX general description

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- MYRRHA PHX design presents the following characteristics:
  - Heat exchange mostly limited to the PHX “active length” (~2.1m) placed between inlet and outlet
  - Well developed two-phase flow inside the PHX tubes from the inlet up to the top
  - High aspect ratio (L/D) providing a better counter-current flow development through the bundle
  - Only one tube plate located under LBE
  - Easier inspection and repair

# MYRRHA PHX general description

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- Potential disadvantages coming from such design approach:
  - High two-phase pressure drop in the tube bundle, with potential increase of dynamic instabilities
  - Notable tube length (~11m) possibly generating important mechanical stresses (weight and thermal induced) in the tube plates and vibrational stresses in the tube bundle
  - Tube bundle in contact with the free surface level leading to possible problems due to differential thermal expansion and level fluctuations  
→ thermal fatigue

# Main analysis findings and outcome

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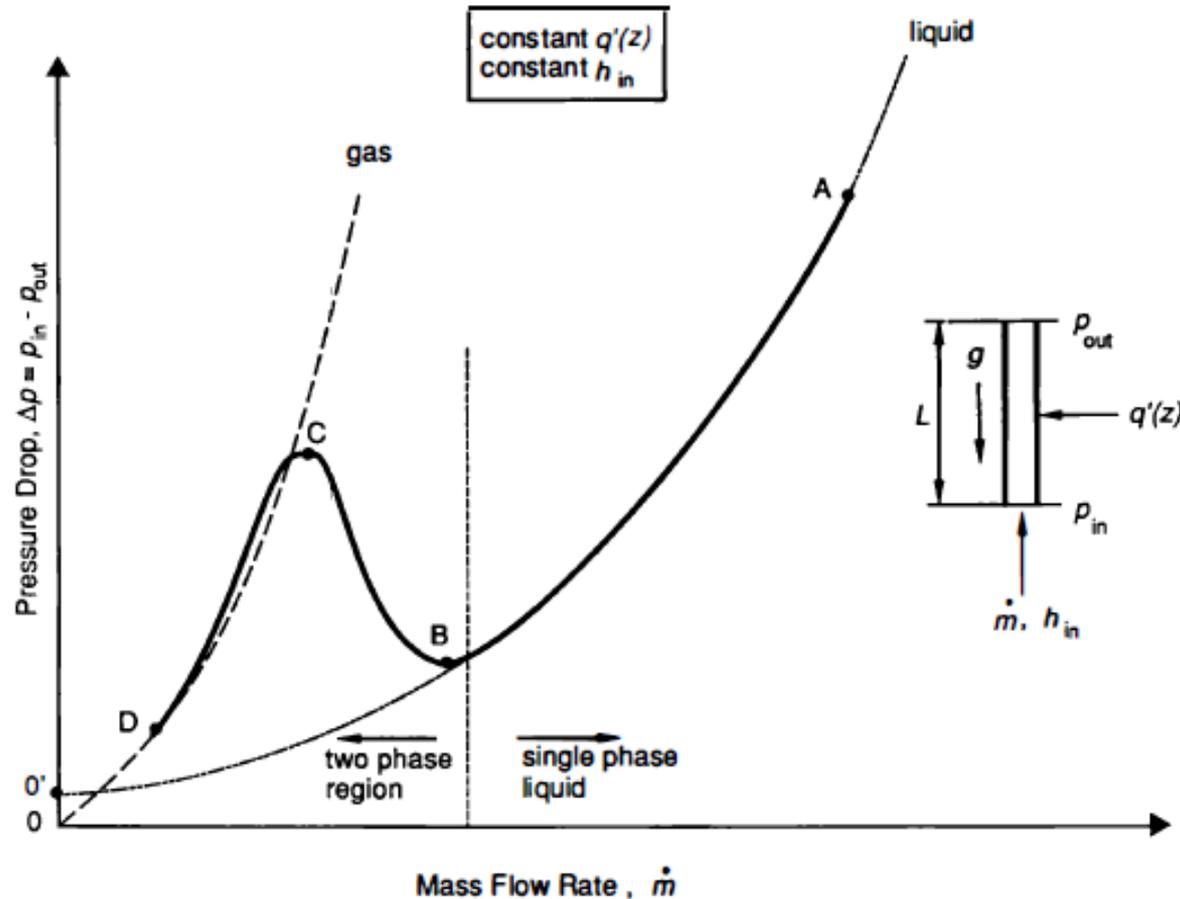
- MYRRHA PHX presents the following main features:
  - Ledinegg instability not a concern because of the low exit quality
  - DWO instability appearing in the system because of the limited water subcooling temperature and the extended two-phase region
  - Partial instability between certain  $Q/m$  intervals where slug flow regime prevails in the active tube section
- By placing an orifice with a diameter  $\sim 4.7$  mm, it is possible to limit to some extent the unstable behavior of the system
- Induced instabilities do not respect the chosen stability criterion
  - A design modification (or a different stability criterion) should be considered

# Two-phase flow instabilities

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- Two kinds of instabilities can be found in a boiling ( $2\phi$ ) tube bundle of an HX:
  - Static instability
  - Dynamic instability
- Among these, three instability types identified for MYRRHA PHX:
  - Ledinegg instability: region of  $\Delta p$ - $m$  characteristic curve allowing for more than a single solution, not always stable
  - Density wave instability: triggered by difference in density between the subcooled liquid entering the channel and the two-phase mixture exiting  $\rightarrow$  transient inertia, lags and feedbacks between boiling channel parameters (mass flow rate, vapor generation rate, pressure drop)
  - Flow regime-induced instability: caused by extended operation in specific flow regimes

# Ledinegg instability

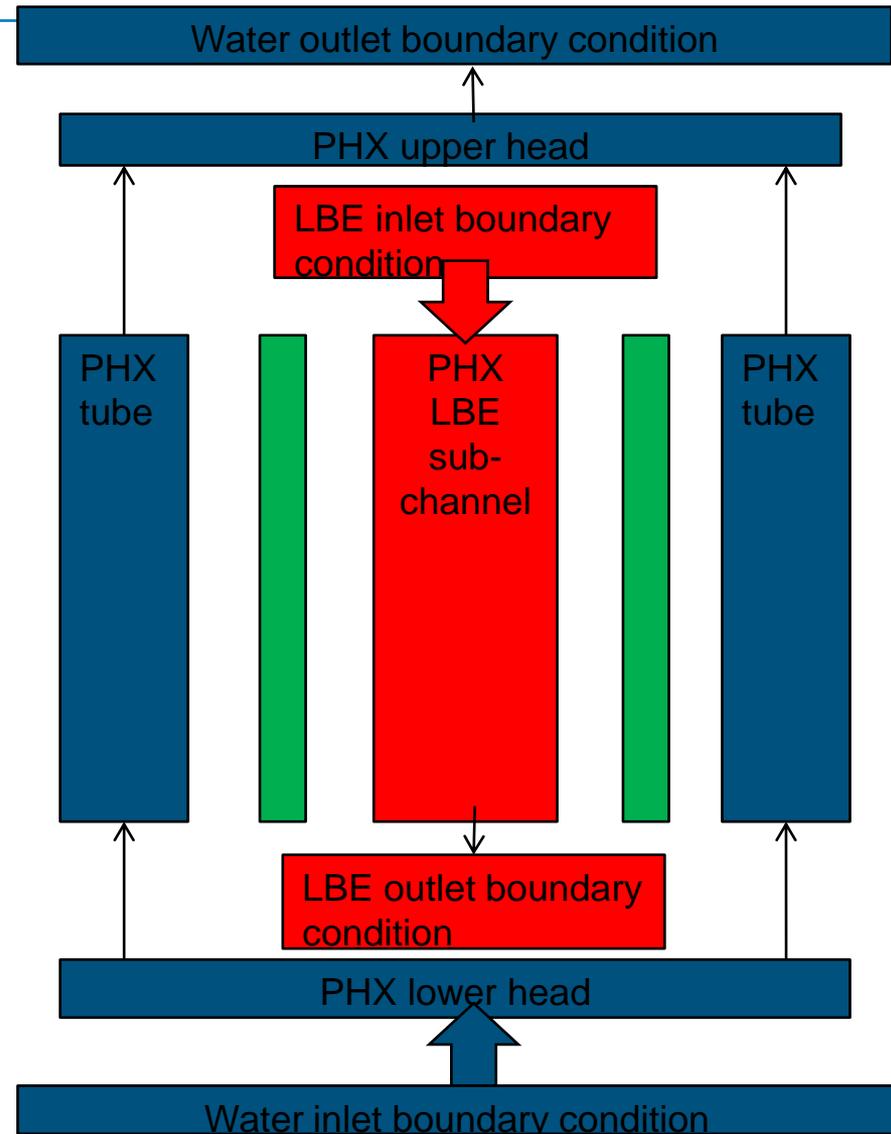


- Region A-B and region C-D: stable ( $\sim$ parabolic characteristic)
- Region B-C: unstable (operating point drifting toward B or C in case of perturbation)

- Ledinegg instability studied through analytical models
- System experiencing Ledinegg instabilities in conditions far from normal operation ( $< 25\%$  mass flow rate)
- Stability assured by low exit quality ( $\sim 0.3$ )
- In all the operating conditions, the working point of the system falls in a perfectly stable range:
  - Mass flow rate per tube:  $0.07 \text{ kg/s}$
  - Tube pressure drop:  $0.95 \text{ bar}$
- DHR conditions: PHX power input considerably lower than normal operation  $\rightarrow$  Ledinegg instability not an issue

# Density wave oscillation instability

- DWO instabilities studied through RELAP5-3D simplified model
  - Real geometry has been assumed for PHX tubes:
    - Correct dimensions
    - Correct local pressure drop factors (Idel'chik)
- Not good response from the DWO instability analysis
  - Nominal flow and subcooling conditions: ~ 60% maximum power
  - Increased subcooling: < 10% maximum power



# Density wave oscillation instability – Parameters effect

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- General effects of different parameters on system stability against DWO instabilities:
  - Outlet quality increase has always a destabilizing effect → thermal power increase and/or mass flow rate decrease have a destabilizing effect
  - Inlet subcooling increase has a stabilizing effect at high subcoolings but a destabilizing effect at low subcoolings
  - System pressure increase has a slight stabilizing effect but, causing also other variations, the final outcome is not obvious
  - Inlet throttling (in monophasic region) increases stability
  - Outlet throttling (in two-phase region) reduces stability

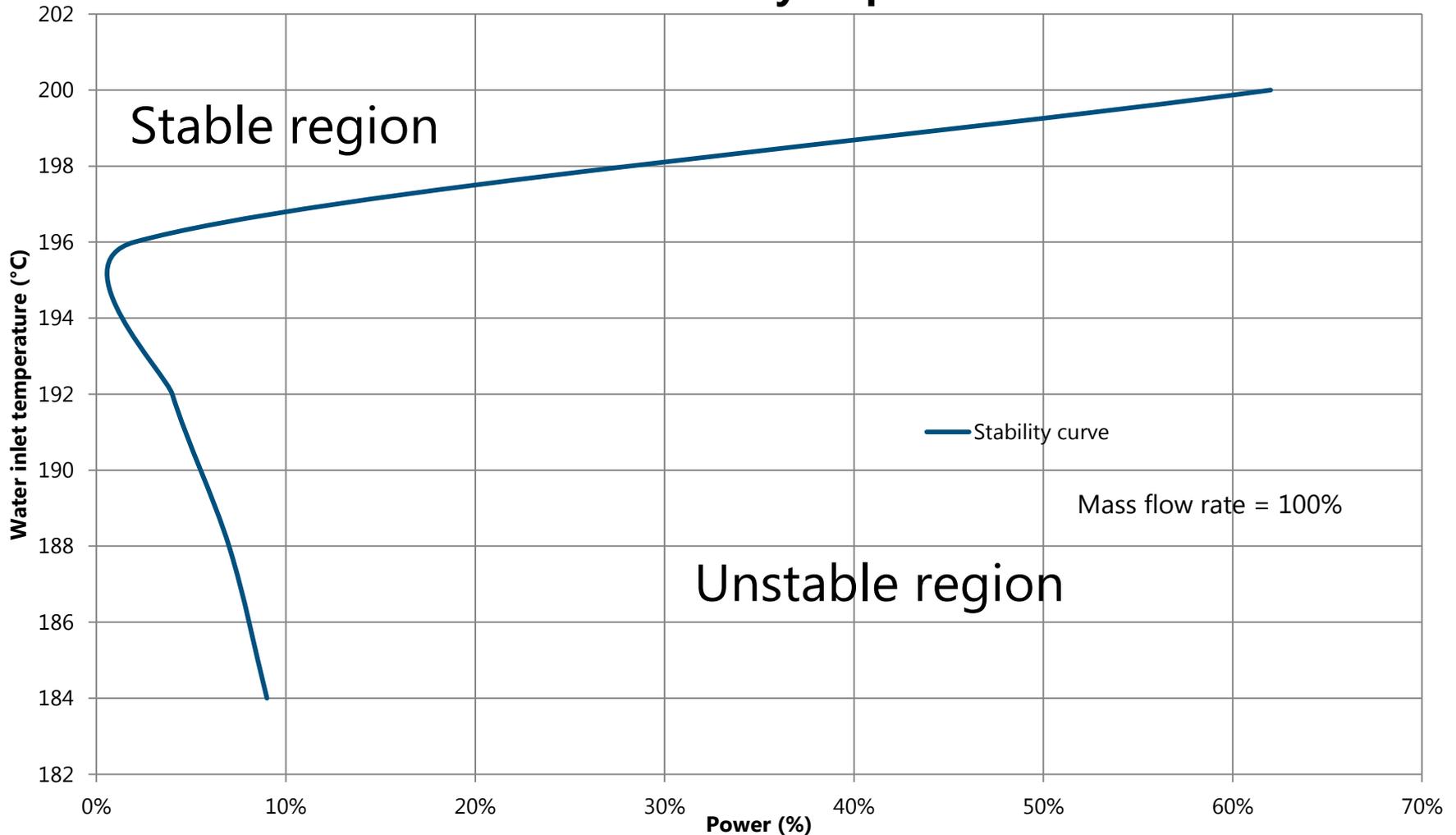
# Density wave oscillation instability – Parameters effect

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- Non-dimensional numbers introduced to account for all parameters' variations in a 2-D representation:
  - Phase change number ( $N_{pch}$ ):
    - $N_{pch} = \frac{q}{m \cdot h_{lv}} * \frac{v_{lv}}{v_l}$
  - Subcooling number ( $N_{sub}$ ):
    - $N_{sub} = \frac{h - h_f}{h_{lv}} * \frac{v_{lv}}{v_l}$
- Advantages of the non-dimensional numbers use:
  - Possibility to include all the parameters' effects through ratios
  - Only two numbers required

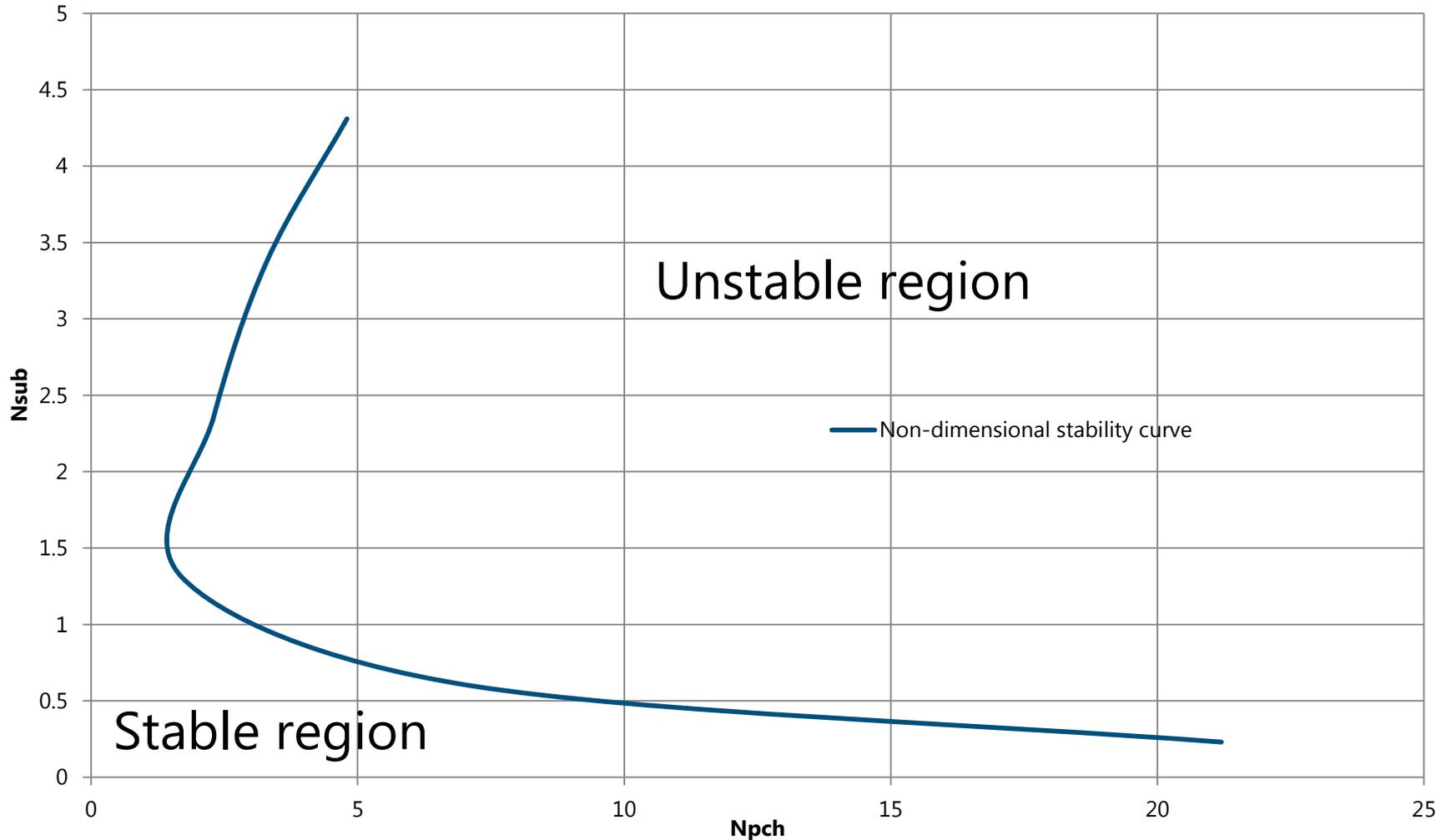
# Density wave oscillation instability

## PHX stability map



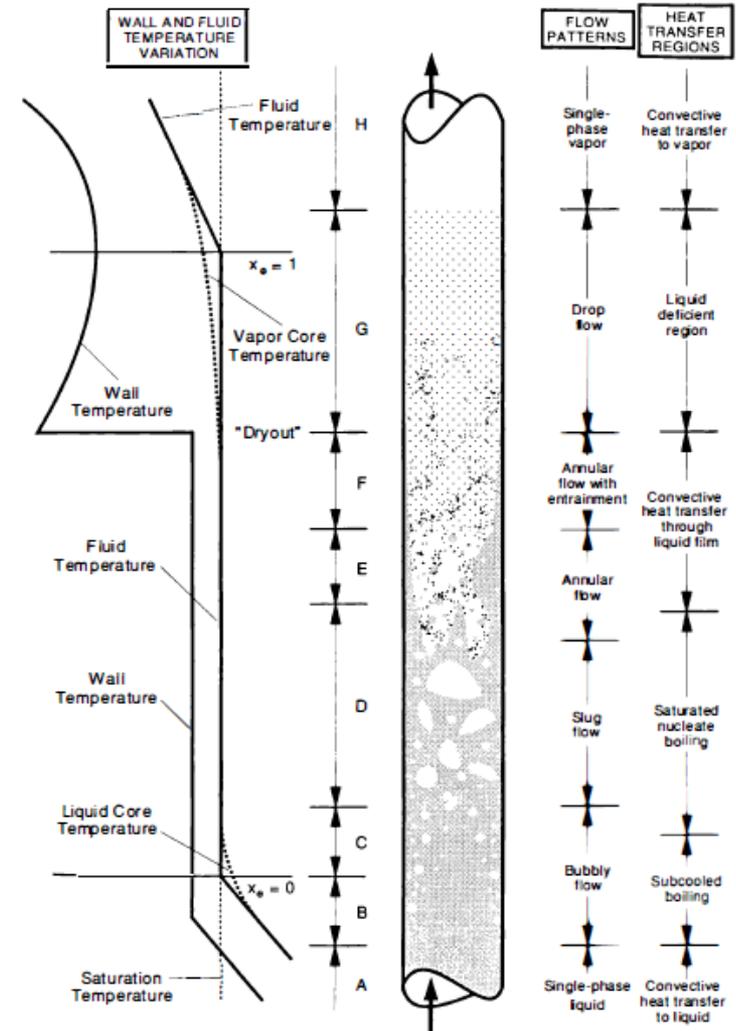
# Density wave oscillation instability – Stability map

## PHX non-dimensional stability map



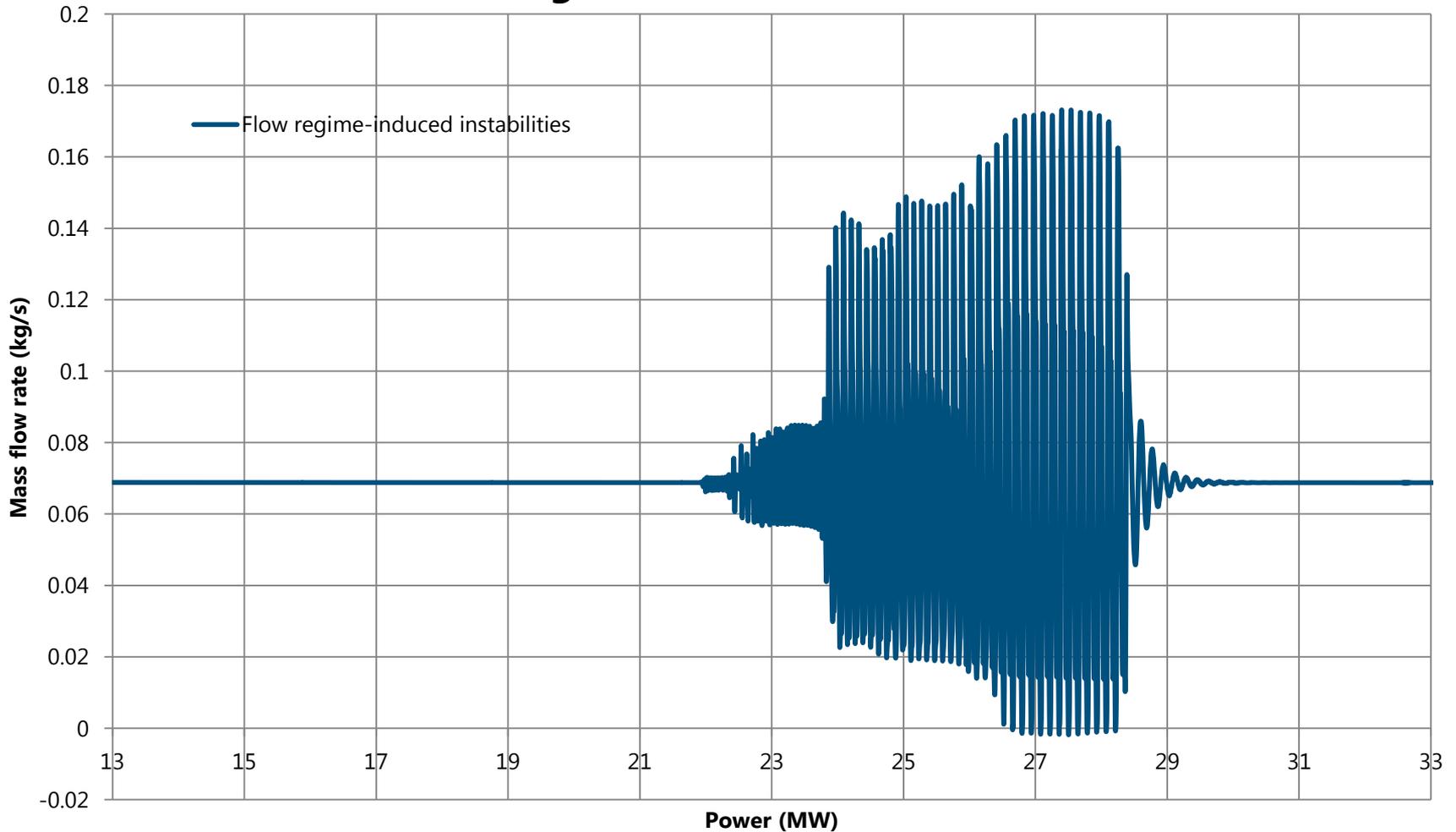
# Flow regime-induced instabilities

- In case PHX active length majority is in two-phase slug flow regime (certain  $Q/m$  specific interval, function of subcooling)  $\rightarrow$  channel flow becomes unstable
- Annular flow more stable  $\rightarrow$  reducing flow (or increasing power) resolves flow-induced instability
- Important for low power operation or for start-up sequence



# Flow regime-induced instabilities

## Flow regime-induced instabilities

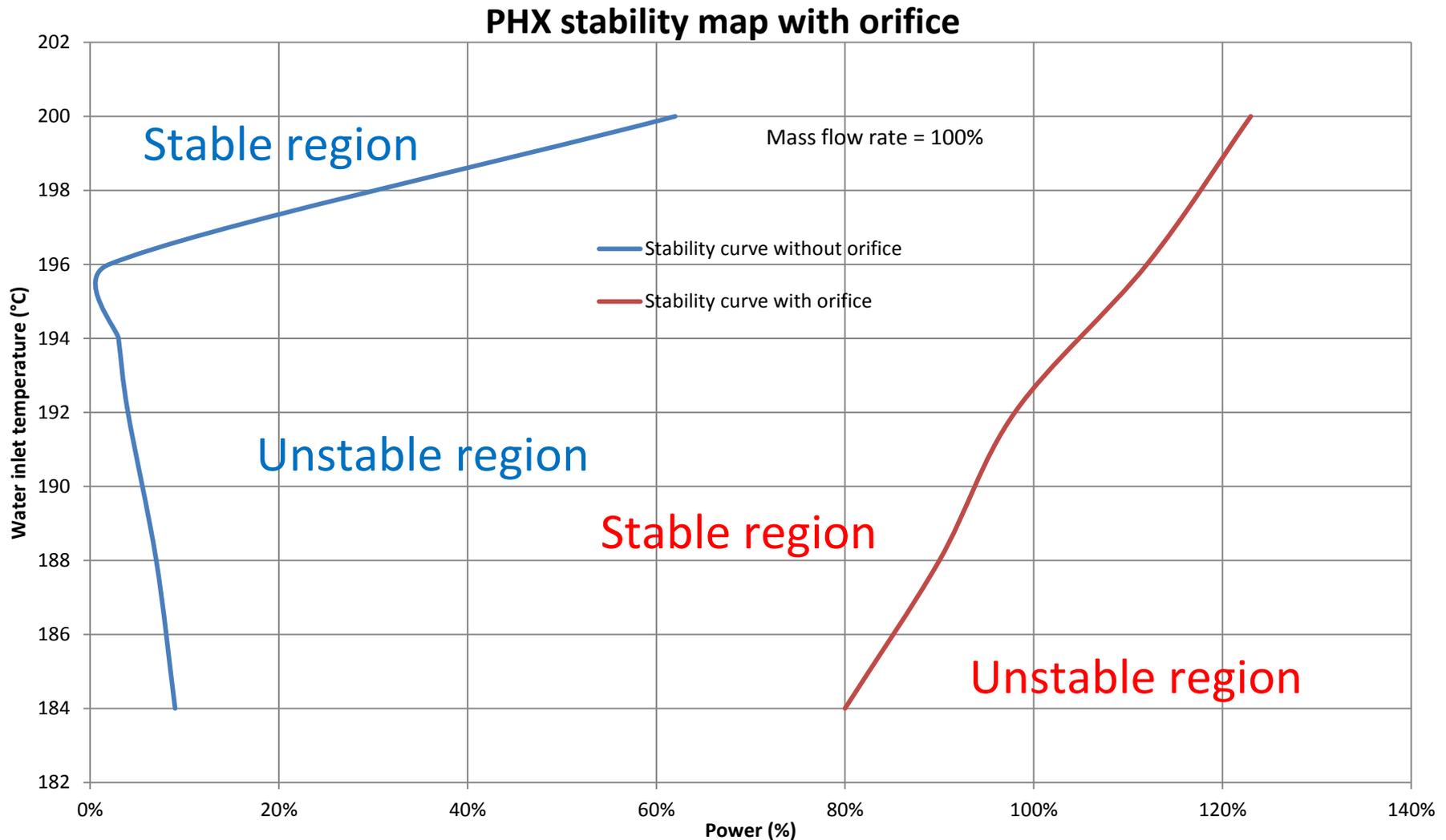


## Towards stability – Orifice dimensioning

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- To avoid DWO instabilities, usual best practice solution is increasing the local pressure drop in the monophasic region → placing an orifice at tube inlet
- By assuming a local pressure drop factor  $K = 120$ , an orifice with the following dimensions has been identified (Idel'chik):
  - Length = 80 mm (same as lower tube plate)
  - Diameter =  $\sim 4.7$  mm ( about 30% of tube diameter)
- Stability map is shifted towards right (increased stability range)
- Little influence found by further increase of orifice local  $K$  factor (→ reducing orifice diameter) beyond  $K = 120$ , but potential problems with local water velocity

# Towards stability – Stability map with orifice



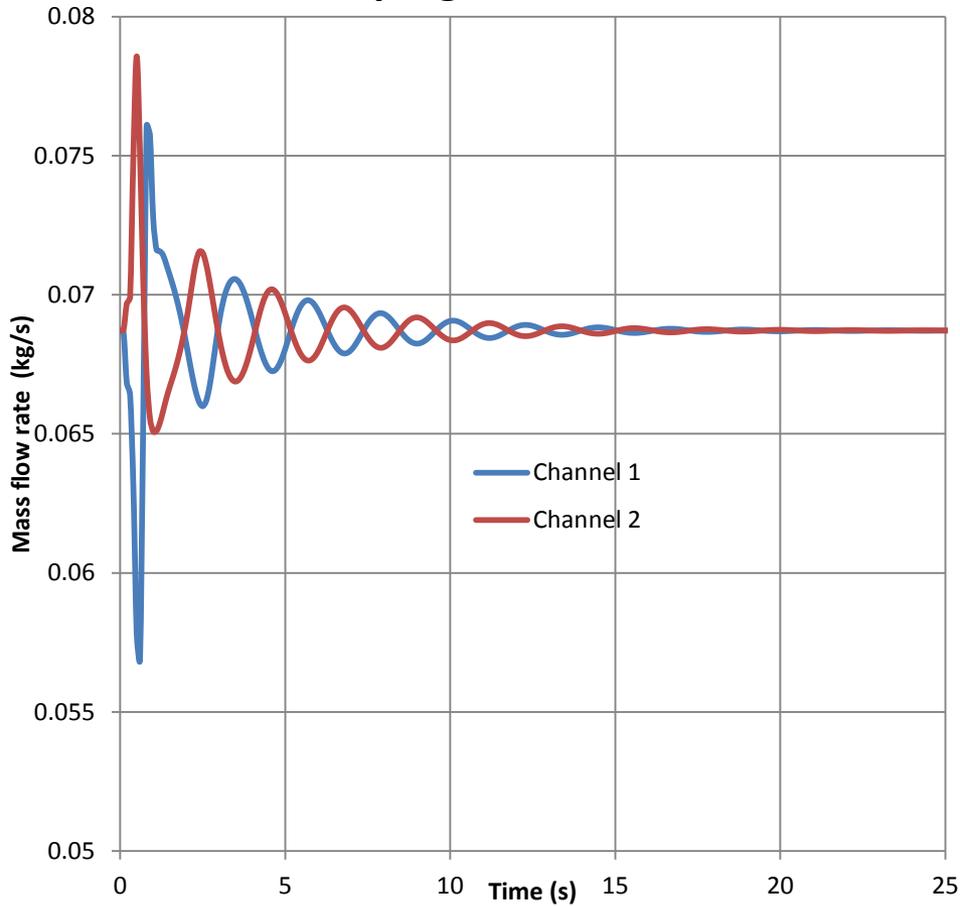
## Induced instabilities – Stability criterion

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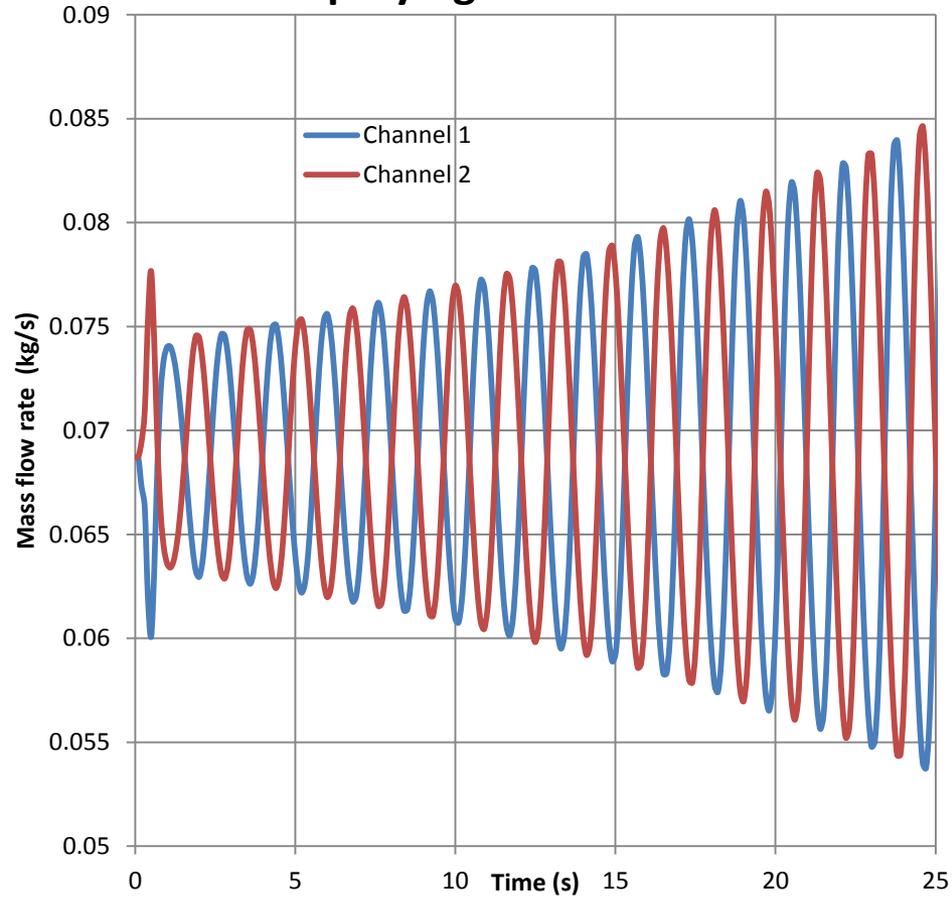
- Resolving (or mitigating) different instabilities is not enough
- Additional design requirement: stability to induced perturbation
  - Local mass flow rate disturbances
  - Local power spikes
- An induced instability usually appears at power levels found to be stable for DWO
- Possible consequences:
  - Amplifying oscillations
  - Damping oscillations
- Stability criterion proposal (from BWR technology):
  - $X_2/X_0 < 0.25$  ( $X_n$  = amplitude of oscillations)
- Mass flow rate perturbation simulated through a valve placed at inlet of one channel and experiencing a closing cycle shaped as half-cosine (0.4 s)

# Induced instabilities – Typical profile

## Damping oscillations

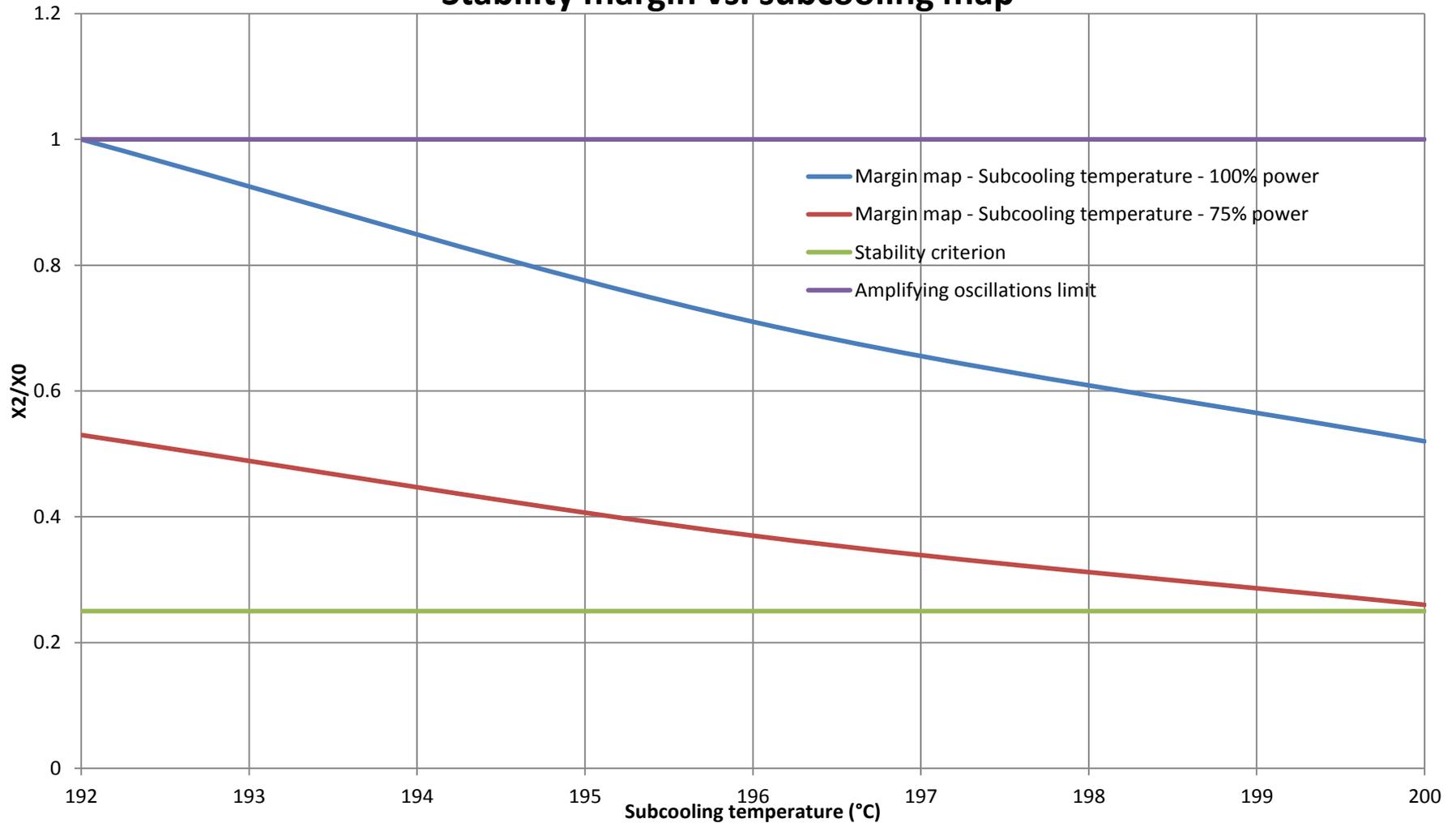


## Amplifying oscillations



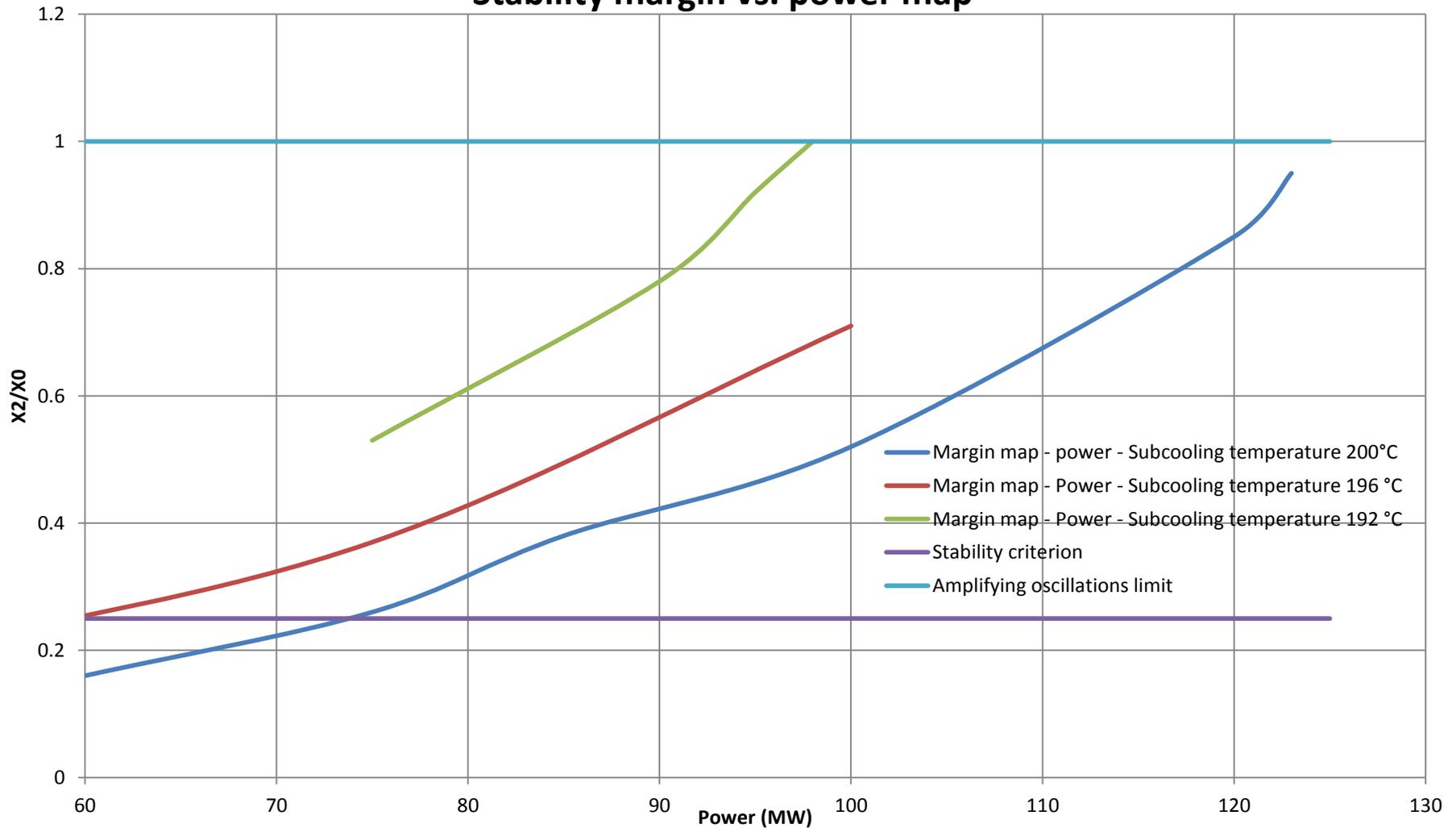
# Induced instabilities – Margin map vs. subcooling

## Stability margin vs. subcooling map



# Induced instabilities – Margin map vs. power

## Stability margin vs. power map



## Induced instabilities – Outcome

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- Stability to induced perturbations is obtained in all normal operation conditions (with orifice  $K = 120$ )
- Respect of induced instability criterion (with orifice  $K = 120$ ) is only possible in specific conditions
- Induced oscillations become amplified in case of:
  - Subcooling  $< 192$  °C
  - Power  $> 123\%$
- Potential solutions:
  - Adoption of new (less stringent) criterion
  - Design modifications

# Main analysis findings and outcome

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- MYRRHA PHX presents the following main features:
  - Ledinegg instability not a concern because of the low exit quality
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## Conclusions and recommendation

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- MYRRHA PHX behavior against instabilities is overall satisfactory
- Parameter values relatively far from the nominal conditions must be avoided
- Recommendation from stability analysis:
  - Avoid the slug flow regime during normal operation through adoption of suitable  $Q/m$  values at all times
  - Obtain a relatively low subcooling temperature at the PHX inlet through pressure losses and/or heat sources in the feedwater line

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Studiecentrum voor Kernenergie  
Centre d'Etude de l'Energie Nucléaire  
Belgian Nuclear Research Centre

Stichting van Openbaar Nut  
Fondation d'Utilité Publique  
Foundation of Public Utility

Registered Office: Avenue Herrmann-Debrouxlaan 40 – BE-1160 BRUSSELS

Operational Office: Boeretang 200 – BE-2400 MOL



STUDIECENTRUM VOOR KERNENERGIE  
CENTRE D'ETUDE DE L'ENERGIE NUCLEAIRE